### Article

Controlled proton accessibility through carboxylic-based organic ligands for highly efficient and selective ammonia electrosynthesis



A remarkable electrocatalyst comprising  $Co_3O_4$  nanoparticles modified with doped La atoms and carboxylic-based organic ligands designed to regulate proton accessibility and suppress competing hydrogen evolution reaction in electrochemical nitrate reduction (eNO<sub>3</sub>RR).



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#### Highlights

Carboxylic-based organic ligands-functionalized electrocatalyst

Lanthanum doping introduces active sites with strong affinity for nitrate ions

Carboxylic-based groups form hydrogen bonds with free water

Controlling proton accessibility suppresses competing hydrogen generation

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### Article

### Controlled proton accessibility through carboxylic-based organic ligands for highly efficient and selective ammonia electrosynthesis

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#### **SUMMARY**

Competing hydrogen evolution reaction (HER) and sluggish multi-electron/proton-involved steps are the major obstacles to improving the efficiency and selectivity of electrochemical nitrate reduction to ammonia (eNO<sub>3</sub>RR). Herein, we modified Co<sub>3</sub>O<sub>4</sub> nanoparticles with doped rare-earth La atoms and carboxylic (COO<sup>-</sup>)-based organic ligands. The COO<sup>-</sup> groups efficiently reduce the water activity around the active sites by forming hydrogen bonds, thus controlling proton accessibility and regulating the adsorption selectivity between nitrate ions and protons. Simultaneously, introducing oxygen vacancies through La doping establishes active sites with a strong affinity for nitrate ions and an electron-rich local environment conducive to eNO<sub>3</sub>RR. The electrocatalyst exhibits superior activity and selectivity with an ammonia Faradaic efficiency of up to 99.41% and a yield rate of 5.62 mg h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup> at -0.3 V vs. reversible hydrogen electrode (RHE). Notably, the catalyst maintains over 90% Faradaic efficiency for NH<sub>3</sub> production across a broad potential range of 400 mV, surpassing most recently reported eNO<sub>3</sub>RR electrocatalysts.

#### INTRODUCTION

Ammonia (NH<sub>3</sub>) is paramount as a widely produced chemical, playing a vital role as building blocks across diverse products, including fertilizers, textiles, and pharmaceuticals.<sup>1</sup> The most typical method for industrialized NH<sub>3</sub> production relies on the Haber-Bosch process, which demands the fusion of nitrogen (N<sub>2</sub>) and hydrogen (H<sub>2</sub>) under formidable conditions of high pressure (200-350 atm) and temperature (400°C-600°C), and large amounts of carbon dioxide (CO<sub>2</sub>) are inevitably generated.<sup>2,3</sup> Due to the burgeoning environmental concerns, extensive research is being performed to explore alternative green routes for NH<sub>3</sub> production, such as electrochemical reduction from N<sub>2</sub> or nitrate (NO<sub>3</sub><sup>-</sup>).<sup>4,5</sup> However, the low NH<sub>3</sub> production rate of electrochemical N<sub>2</sub> reduction accentuates the interest in NO<sub>3</sub><sup>-</sup> reduction.<sup>6,7</sup> Meanwhile,  $NO_3^-$  usually exists in industrial and agricultural wastewater, leading to environmental and health issues.<sup>8,9</sup> The incomplete conversion of  $NO_3^{-1}$  into nitrites  $(NO_2^{-})$  also brings health concerns, while the reduction into N<sub>2</sub> is energy intensive (about 11.7–12.5 kWh kg N<sup>-1</sup>),<sup>10</sup> so electrochemical nitrate reduction reaction to NH<sub>3</sub> (eNO<sub>3</sub>RR) become a significant scientific research hotspot. The eNO<sub>3</sub>RR meets the requirements for removing nitrate ions from wastewater and efficiently produces high-value-added NH<sub>3</sub>.<sup>11</sup> Nevertheless, the rational design of electrocatalysts for eNO<sub>3</sub>RR with both high selectivity and activity is still lacking, especially since there is a competing hydrogen evolution reaction (HER) that is only a two-electron transfer process.<sup>12</sup>



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Ammonia, the second most popular commercialized synthetic chemical in the world, is widely used for fertilizer and production of all nitrogen-atom-containing chemicals. Electrochemical nitrate reduction reaction (eNO<sub>3</sub>RR) offers a green and appealing approach to sustainable ammonia synthesis. However, it is hindered by the multi-proton-coupled electron transfer steps and competitive hydrogen evolution reaction (HER). To this end, keeping an appropriate equilibrium of electron and proton accessibility kinetics around the active sites of catalysts emerges as a crucial principle to enhance the activity and selectivity of eNO<sub>3</sub>RR. In this work, we demonstrate that the carboxylic-based organic ligands on metal oxides could form hydrogen bonds with water, effectively diminish water activity, and control the proton accessibility, thus achieving a highly efficient and selective ammonia electrosynthesis.





In general, the eNO<sub>3</sub>RR process involves three stages: (1) the adsorption of NO<sub>3</sub><sup>-</sup> on the active sites, (2) the continuous proton-coupled electron transfer (PCET) steps including nine protons and eight electrons (NO<sub>3</sub><sup>-</sup> + 9H<sup>+</sup> + 8e<sup>-</sup>  $\rightarrow$  NH<sub>3</sub> + 3H<sub>2</sub>O in acidic and neutral electrolytes or NO $_3^-$  + 6H $_2$ O + 8e $^ \rightarrow$  NH $_3$  + 9OH $^-$  in alkaline electrolytes), followed by (3) the formation and desorption of  $NH_3$  molecules.<sup>13–15</sup> Basically, the adsorption and desorption rely on the intrinsic activity of the active sites, while PCET steps mainly depend on the electron and proton accessibilities.<sup>16,17</sup> Besides, the competing HER that lies on the adsorption priority of  $NO_3^+$  and  $H^+$  on active sites also significantly influences the eNO<sub>3</sub>RR rate. Therefore, it follows that the electron and proton accessibility-kinetic profoundly governs the pace of the PCET step and remains pivotal in curtailing the generation of undesirable by-products, such as H<sub>2</sub>. For example, semimetals such as Sn and Bi have recently been introduced as sub/monolayer second metals on the electrodes to suppress HER and promote nitrate adsorption due to the reported limited electron transfer and weakened hydrogen binding on the surface.<sup>18-20</sup> Nonetheless, an excessive hindrance of electron or proton supply unavoidably results in a shortage of essential resources for the eNO<sub>3</sub>RR process. In this regard, keeping an appropriate equilibrium of electron and proton accessibility kinetics at the surface of catalysts emerges as a crucial principle. This principle offers valuable direction for current research and development efforts on the optimal design of eNO<sub>3</sub>RR electrocatalysts with high activity and selectivity.

With regard to the competing HER, although nitrate reduction can happen at an overpotential lower than HER, the reaction would then occur under a small current density, and the NH<sub>3</sub> synthesis remains considerably distant from achieving an industrial scale.<sup>21,22</sup> This discrepancy underscores a crucial challenge: effectively curb hydrogen generation while achieving increased NH<sub>3</sub> production under high overpotentials. Recent strides in research have entailed the introduction of additives, such as dimethyl sulfoxide (DMSO), hydrophilic polyethylene glycol (PEG), and glucose, into the aqueous electrolyte.<sup>23-25</sup> This strategic modification diminishes water activity by forming hydrogen bonds (H-bonds) between the additives and the free water molecules. However, the eNO<sub>3</sub>RR process still depends on water splitting in aqueous media as a proton donor to supply continual generation of active adsorbed hydrogen (\*H [the asterisk represents the active sites]), which needs to be regulated to a balanced level. Electrolyte additives, especially in high concentrations, can easily go beyond the limit and thus retard the water splitting. Consequently, rational strategies must be developed to control HER rate but not affect proton supply. Inspired by the function of organic electrolyte additives, organic molecule ligands or even organic molecules have attracted intensive interest in electrocatalysis. This paradigm shift toward organic molecules underlines their promise in addressing the intricate balance between HER control and maintaining an adequate proton reservoir. For instance, Chen et al. reported an excellent performance of a single ethylenediaminetetraacetic acid (EDTA) molecular catalyst for reducing CO<sub>2</sub> to CH<sub>4</sub>.<sup>26</sup> They found that the Lewis basic carboxylic (COO<sup>-</sup>) groups act as the active sites for CO<sub>2</sub> reduction and have favorable energy for the hydrogenation of \*CO to the reduced product of CH<sub>4</sub>. Despite density functional theory (DFT) calculations proving the excellent electrocatalysis performance of organic molecules in these works, there are few reports on the application of eNO<sub>3</sub>RR. Furthermore, challenges remain in terms of how the organic functional groups affect the electronic structure of active sites and the transfer of protons, and the relationship between the selectivity of eNO<sub>3</sub>RR and suppressed HER is still ambiguous.

In this work, we take the electron-rich carboxylate functional group as an example and elucidate the significant effect of carboxylate groups on confining the water <sup>1</sup>Department of Materials Science and Engineering, City University of Hong Kong, Hong Kong, Hong Kong SAR 999077, China

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activity, facilitating nitrate adsorption, and balancing the PCET steps in eNO<sub>3</sub>RR. Lanthanum (La), a rare-earth element, is doped into Co<sub>3</sub>O<sub>4</sub> nanoparticles (NPs). Taking advantage of a larger ionic radius than Co, unique Lewis acid characteristics, and high coordination number of La, the La doping leads to the lattice disorder of  $Co_3O_4$ NPs and generates abundant oxygen vacancies (O<sub>v</sub>) while serving as a bridge to combine Co<sub>3</sub>O<sub>4</sub> with carboxylic-based organic ligands, which function as Lewis bases.<sup>27</sup> Electrochemical in situ measurements, including attenuated total reflection surface-enhanced infrared absorption spectroscopy (ATR-SEIRAS) measurement, Raman spectroscopy measurement, and differential electrochemical mass spectrometry (DEMS) test as well as density functional theory (DFT) calculations and molecular dynamics (MD) simulations conducted to demonstrate the reduced water activity and clarify the PCET mechanisms and pathways during eNO<sub>3</sub>RR. The resulting carboxylate-functionalized La-doped Co<sub>3</sub>O<sub>4</sub> catalysts exhibit superior catalytic performances, (1) exhibiting a Faradaic efficiency (FE) as high as 99.41% with an NH<sub>3</sub> yield rate of 5.62 mg  $h^{-1}$  mg<sub>cat</sub><sup>-1</sup> at -0.3 V vs. reversible hydrogen electrode (RHE), (2) achieving the  $\rm NH_3$  yield rate of 31.24 mg  $\rm h^{-1}~mg_{cat}^{-1}$  at -0.7 V vs. RHE, and (3) possessing a wide potential window (400 mV, from -0.3 to -0.7 V) for NH<sub>3</sub> production with >90% FE, which is top-ranked among the electrocatalysts for eNO<sub>3</sub>RR so far. This work provides a rational strategy based on organic carboxylic ligands for the high NH<sub>3</sub> production rate. More importantly, the findings can contribute to subsequent catalyst optimization and scaling up in other electrochemical techniques with HER as a competition reaction, such as CO<sub>2</sub> reduction.

#### **RESULTS AND DISCUSSION**

#### Synthesis and structural characterizations

Co<sub>3</sub>O<sub>4</sub> NPs were synthesized by a simple coprecipitation method, employing cobalt nitrate hexahydrate (Co(NO<sub>3</sub>)<sub>2</sub> $\cdot$ 6H<sub>2</sub>O) and sodium hydroxide (NaOH) as reactants. The La-doped  $Co_3O_4$  catalysts with rich oxygen vacancies (La- $Co_3O_{4-x}$ ) were fabricated using an identical procedure, with the exception that lanthanum nitrate hexahydrate (La(NO<sub>3</sub>)<sub>3</sub>·6H<sub>2</sub>O) was included in the precursor. The abbreviation La<sub>v</sub>- $Co_3O_{4-x}$  (where y = 3, 6, and 9) represents  $Co_3O_{4-x}$  with different La doping concentrations of 3.02, 6.29, and 9.11 atom % (La-Co<sub>3</sub>O<sub>4-x</sub> represents La<sub>9</sub>-Co<sub>3</sub>O<sub>4-x</sub> in the following). Figure 1A depicts the schematic illustration of the crystal structure evolution of Co<sub>3</sub>O<sub>4</sub> studied here. The spinel Co<sub>3</sub>O<sub>4</sub> adopts the standard spinel structure with  $Co^{2+}$  ions in the tetrahedral coordination centers (A<sub>td</sub>, yellow block) and  $Co^{3+}$ ions in the octahedral interstices (B<sub>oh</sub>, violet block), thus allowing the Co<sub>3</sub>O<sub>4</sub> crystal with internal corner-sharing  $A_{td}{-}O{-}B_{oh}$  and edge-sharing  $B_{oh}{-}O{-}B_{oh}$  configurations.<sup>28,29</sup> As reported, the substitution of Co<sup>3+</sup> by La<sup>3+</sup> for the occupation of the B<sub>ob</sub> sites occurs more readily. However, the significant mismatch of the ionic radius between La<sup>3+</sup> and Co<sup>3+</sup> may result in strong lattice strain, thereby leading to the rearrangement of  $A_{td}$  and  $B_{oh}$  sites and the formation of oxygen vacancies ( $O_v$ ).<sup>30</sup> DFT calculations have been utilized to determine the formation energy in both substitution situations (Figure S1). The outcomes coincide with previously reported findings, affirming that the replacement of Boh by La yields lower formation energy than the Atd substitution. After that, we choose benzenetricarboxylic acid (H<sub>3</sub>BTC) with three carboxylates as carboxylic organic ligands. Leveraging the unique Lewis acid attributes and high coordination number of the rare-earth element La,<sup>31</sup> its incorporation serves as a bridging mechanism connecting the carboxylate functional ligand with  $Co_3O_4$  (abbreviated as BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, in which La-Co<sub>3</sub>O<sub>4-x</sub> represents La<sub>9</sub>- $Co_3O_{4-x}$ ). The as-prepared BTC/La-Co<sub>3</sub>O<sub>4-x</sub> NPs show an average size of 14.37  $\pm$ 5.28 nm, which is a little smaller than that of  $Co_3O_4$  NPs (19.97  $\pm$  7.10 nm), resulting from the larger ionic radius of dopant atoms than host atoms (Figures 1B, 1C,





Figure 1. Schematic illustration and structural characterization for the preparation of BTC/La- $Co_3O_{4-x}$  and reference materials (A) Schematic illustration of the crystal structures of  $Co_3O_{4-x}$  and  $BTC/La-Co_3O_{4-x}$ .

(B) TEM image of  $\rm Co_3O_4$ , and the inset shows the corresponding SAED pattern.

(C) TEM image of BTC/La-Co $_{3}\text{O}_{4\text{-x}}$  and the inset shows the corresponding SAED pattern.

(D) XRD patterns of Co $_3O_4$ , La-Co $_3O_{4\text{-}x\text{,}}$  and BTC/La-Co $_3O_{4\text{-}x\text{.}}$ 

(E) HRTEM image of Co<sub>3</sub>O<sub>4</sub>.

(F) HRTEM image of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>.

(G) Inverse FFT image from the region circled by the yellow dashed box in (F).

and S2).<sup>32</sup> The insets in Figures 1B and 1C are the corresponding selected area electron diffraction (SAED) patterns, revealing that the lattice spacings of both the samples are well consistent with the cubic phase of  $Co_3O_4$  (JCPDS 42–1467) in the X-ray diffraction (XRD) patterns and no other La-based compounds are formed (Figure 1D). Based on Figure S3A, it is important to highlight that the peak intensities significantly decrease as the La doping content increases, along with the introduction of BTC ligands. This phenomenon arises due to the differing electron densities between the introduced atoms (La atoms) and their surrounding counterparts, reducing crystallinity and increasing defect occurrence.<sup>32</sup> Additionally, the amplified area from Figure S3A shows a slight peak shift to a lower angle with the increased La doping because the lattice expansion resulted from the replacement of  $Co^{3+}$  by La<sup>3+</sup> with a bigger ionic radius.<sup>33</sup> The g-value signals at 2.002 of electron paramagnetic resonance (EPR) related to oxygen vacancies are detected for La<sub>y</sub>-Co<sub>3</sub>O<sub>4-x</sub>, verifying the formation of O<sub>v</sub> due to the La doping (Figure S3B).<sup>34</sup> Additionally, this augmented O<sub>v</sub> content is also shown by the reduced Raman peak intensity and broader peak



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width in Figure S4.<sup>35</sup> Figures 1E and S5 display the high-resolution transmission electron microscopy (HRTEM) image of pure  $Co_3O_4$  NPs, which indicates good crystallinity with typical (220) facets in the cubic phase. Upon modification with La atoms and BTC ligands, although the lattice spacings of the  $Co_3O_4$  (311) plane of 2.437 Å are discernible, a majority of the lattice fringes become less distinctive (Figures 1F and S6). These dislocations and distortions are even more apparent following the application of an inverse fast Fourier transform (FFT) mask to the selected region, further demonstrating the incorporation of numerous  $O_v$  defects within the lattice (Figure 1G). These  $O_v$  defects equalize electron distribution, compensating for the uneven electron density resulting from La doping and leading to unsaturated coordination at both La and Co sites. This distribution ensures the requisite coordination environment for BTC ligands, culminating in a substantial augmentation of active sites,<sup>36</sup> which will be substantiated by subsequent experimental investigations.

The zeta ( $\zeta$ ) potential represents the charge that develops at the boundary between an NP surface and the surrounding liquid medium. It stands as an important technique for comprehending the state of the NP surface.<sup>37,38</sup> As shown in Figure 2A, both pure Co<sub>3</sub>O<sub>4</sub> and H<sub>3</sub>BTC show a negative charged surface in aqueous solution (pH = 7). Under La doping, the  $\zeta$  potential of Co<sub>3</sub>O<sub>4</sub> NPs transforms from -3.85 to 1.47 mV, manifesting the emergence of the positively charged surface due to the generated surface  $O_{v}$ , which is also beneficial for the combination of electron-rich BTC ligands owing to electrostatic attraction force.<sup>39</sup> As for BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, the  $\zeta$ potential of 1.07 mV is smaller than that of  $La-Co_3O_{4-x}$  because of the addition of negative electrons from the COO<sup>-</sup> of BTC ligands. Despite this, the  $\zeta$  potential remains predominantly positive on the surface of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, ensuring favorable electrostatic adsorption toward NO<sub>3</sub><sup>-</sup> during eNO<sub>3</sub>RR. Furthermore, Fourier transform infrared (FTIR) and Raman spectra were conducted to validate the presence of BTC ligands (Figures 2B and 2C). In addition to the two absorption FTIR peaks at 549 and 658  $\text{cm}^{-1}$ , which correspond to the Co–O bond in the spinel lattice, representing Co<sup>3+</sup> in an octahedral hole, and the O-Co-O bond of Co<sup>2+</sup> in a tetrahedral site, respectively, two distinct peaks at 1,366 and 1,557  $\text{cm}^{-1}$  are observable, which are from symmetric and asymmetric vibrations of -COO<sup>-</sup> (Figure 2B).<sup>40,41</sup> Additionally, two relatively subtle peaks located at 1,436 and 1,669 cm<sup>-1</sup>, signifying the vibrations of -COOH, are observed.<sup>42</sup> These observations align with the characteristic peaks of H<sub>3</sub>BTC. In the meantime, the obvious doublet Raman bands around 1,446 and 1,634 cm<sup>-1</sup> are shown in BTC/La-Co<sub>3</sub>O<sub>4-x</sub> (Figure 2C), belonging to the stretching modes of uncoordinated carboxylate groups. It is noteworthy that these two peaks of stretching modes are broad, which cover the moiety of -COO<sup>-</sup> groups located at 1,610 and 1,424 cm<sup>-1</sup>.<sup>43</sup> Furthermore, the high-angle annular dark-field (HAADF) image and energy dispersive spectrometry (EDS) elemental mapping (Figure 2D), scanning electron microscope (SEM)-energy dispersive X-ray (EDX) spectra, and EDS elemental mapping (Figures S7, S8, S9, and S10) demonstrate a uniform distribution of La and C elements throughout the samples after La doping and H<sub>3</sub>BTC combination. The above results, taken together, confirm the successful synthesis of Lav-Co<sub>3</sub>O<sub>4-x</sub> and BTC/La-Co<sub>3</sub>O<sub>4-x</sub> NPs.

More importantly, the electronic structures and local environment are explored by the charge density differences, Bader charge, X-ray photoelectron spectroscopy (XPS), and X-ray absorption spectroscopy for the catalysts. As depicted in Figures 2E and S11, La-Co<sub>3</sub>O<sub>4-x</sub> exhibits robust electronic interactions around the La atom, donating 0.16e to neighboring O atoms. Furthermore, a conspicuous charge depletion is observable in the O<sub>v</sub> region, while the electrons accumulate at



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Figure 2. Characterization of the BTC ligand and electronic microenvironment of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> and reference materials

(A) Zeta ( $\zeta$ ) potential in aqueous solution (pH = 7).

(B) FTIR spectra.

(C) Raman spectra.

(D) HAADF image and EDS elemental mapping of BTC/La-Co $_3\mathrm{O}_{4\text{-}x\text{-}}$ 

(E) Charge density differences and charge transfer of La-Co<sub>3</sub>O<sub>4-x</sub> with the cyan and yellow colors designating the depletion and accumulation of charge density. (F) Charge density differences and charge transfer of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> with the cyan and yellow colors designating the depletion and accumulation of charge density.

(G) The  $Co^{2+}/Co^{3+}$  atomic ratio, surface Co atomic ratio, and  $O_v/O_{latt}$  ratio on the surface of the samples.

(H) The  $k^3$ -weighted Fourier transform spectra from La L3 edge EXAFS in R space.

(I) Wavelet-transformed  $k^3\mbox{-weighted}$  EXAFS spectra of  $La_2O_3.$ 

(J) Wavelet-transformed  $k^3$  -weighted EXAFS spectra of BTC/La-Co $_3O_{4\mbox{-}x\mbox{-}x}$ 

the adjacent Co and neighboring O atoms in the visual area, of which electron transfer is calculated to be 0.19e and 0.04e. Combined with the BTC ligands, the La atoms serve as a bridge to connect the two O atoms (O<sub>1</sub> and O<sub>2</sub> in Figure 2F) in BTC with the

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O atoms in the  $Co_3O_4$  lattice (Figures 2F and S11). The guantitative amount of electron transfers from BTC to  $Co_3O_4$  is confirmed to be 0.05e. The abundant electrons around the La $-O_v$ -Co sites make it more available to adsorb NO<sub>3</sub><sup>-</sup> due to the sufficient electron supply for back-donating to the antibonding of NO<sub>3</sub><sup>-</sup> orbitals.<sup>35,44</sup> These results verify that introducing La atoms and BTC ligands can modulate the catalysts' electronic structure and charge redistribution, thus, in turn, orchestrating a regulation of the local environment conducive to facilitating efficient nitrate reduction activity. Moreover, the high-resolution Co 2p XPS spectra could be deconvoluted into Co 2p<sub>3/2</sub> and Co 2p<sub>1/2</sub> (779.5 and 794.6 eV for Co<sup>3+</sup>, 780.8 and 795.9 eV for Co<sup>2+</sup>) associated with their satellite peaks (Figure S12A).<sup>45</sup> With the increased doping content of La, the samples exhibit pronounced La  $3d_{5/2}$  and  $3d_{3/2}$  core peaks attributed to the La<sup>3+</sup> species (Figure S13).<sup>46</sup> Besides, the O 1s XPS spectra could be fitted into three prominent peaks at binding energies of about 529.8, 531.5, and 533.3 eV, assigned to the lattice oxygen (O<sub>latt</sub>), oxygen atoms next to their vacancies (O<sub>v</sub>), and oxygen in the molecular water or hydroxyl species adsorbed on the catalyst surface (O<sub>ads</sub>), respectively (Figure S12B).<sup>36</sup> Notably, additional peaks at 530.3 and 532.0 eV in BTC/La-Co3O4-x suggest that the oxygen in C=O and C-O bonds to the carboxylic groups in BTC ligands.<sup>47</sup> Remarkably, a reduction in the binding energies is discernible within the Co 2p and O 1s peaks of La<sub>v</sub>-Co<sub>3</sub>O<sub>4-x</sub>. This shift indicates the electron transfer from the doped La to the host Co<sub>3</sub>O<sub>4</sub> NPs, which is in agreement with the calculated results of charge density differences.<sup>48</sup> By estimating the XPS data, we construct a correlation of the surface Co atom %,  $Co^{2+}/Co^{3+}$ , and  $O_v/O_{latt}$ ratios as a function of the La contents and the incorporation of BTC in BTC/La- $Co_3O_{4-x}$  in Figures 2G and S14 and Table S1. Firstly, the surface Co atom % displays a volcano plot, accompanied by an approximate upward trend in both the  $Co^{2+}/$  $Co^{3+}$  and  $O_v/O_{latt}$  ratios with the increased La doping contents, signifying the substituted  $Co^{3+}$  by La<sup>3+</sup> and the formation of O<sub>v</sub>. In particular, La<sub>9</sub>-Co<sub>3</sub>O<sub>4-x</sub> has the highest  $O_v/O_{latt}$  ratio in comparison with pure  $Co_3O_4$ ,  $La_3-Co_3O_{4-x}$ , and  $La_6$ -Co<sub>3</sub>O<sub>4-x</sub>, implying the abundant surface O<sub>v</sub> induced by the doped La atoms, creating adequate sites for adsorbing the BTC ligands. Therefore, the following investigations choose La<sub>9</sub>-Co<sub>3</sub>O<sub>4-x</sub> as the object. To further confirm the doping of La, X-ray absorption near-edge structure (XANES) and extended X-ray absorption fine structure (EXAFS) spectroscopy are performed in Figures 2H-2J and S15. The close absorption edge energy of normalized XANES spectra for BTC/La-Co<sub>3</sub>O<sub>4-x</sub> and reference La<sub>2</sub>O<sub>3</sub> indicates the +3 valence state of La in BTC/La-Co<sub>3</sub>O<sub>4-x</sub>. Furthermore, the k<sup>3</sup>-weighted Fourier transform spectra in R space and the wavelet transform simulations in k space both indicate the doping of La, with only La-O and La-Co coordination structure in the coordination shell and no La-La scattering path (about 3.8 Å in  $La_2O_3$ ) can be identified in BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, which clearly prove that La is atomic distributed into the lattice of Co<sub>3</sub>O<sub>4</sub>. Meanwhile, the fitting results in Table S2 show that the coordination number for La-O in BTC/La-Co<sub>3</sub>O<sub>4-x</sub> is about 5.4, which is close to but lower than the six coordination in  $CoO_6$  octahedron in Co<sub>3</sub>O<sub>4</sub>, providing direct evidence for the replaced Co<sup>3+</sup> and generated oxygen vacancies.<sup>49</sup> Collectively, these findings offer compelling evidence of electron redistribution and the resultant modulation of the local environment ensuing from the incorporation of La and BTC ligands, laying the foundation for the favorable adsorption energy of  $*NO_3$  and fast conversion from  $*NO_3$  to  $*NO_2$ .

#### Electrochemical activity and kinetics of eNO<sub>3</sub>RR

We then explore the electrochemical performance of  $eNO_3RR$  and evaluate the synergistic effects between La doping and BTC ligands. We detect the potential products using the colorimetric method (Figures S16–S18). Initially, we conduct linear sweep voltammetry (LSV) on all the prepared electrocatalysts in the electrolyte





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#### Figure 3. eNO<sub>3</sub>RR performance of the catalysts

(A) LSV curves.

(B) Faradaic efficiencies (FEs) for NH<sub>3</sub>, NO<sub>2</sub>, and H<sub>2</sub>. Error bars represent the standard deviation from three same samples for testing three times.

(C) FE for H<sub>2</sub>; the inset shows the Tafel slopes during HER. Error bars represent the standard deviation from three same samples for testing three times. (D) Partial current densities of NH<sub>3</sub> (j<sub>NH3</sub>).

(E) Yield rate for NH<sub>3</sub> (Y<sub>NH3</sub>). Error bars represent the standard deviation from three same samples for testing three times.

(F) Comparison of  $Y_{NH3}$  and  $FE_{NH3}$  of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> NPs with the recently reported representatives eNO<sub>3</sub>RR electrocatalysts at different potentials (see also Table S3).

(G) Time-dependent current density curves and corresponding Y<sub>NH3</sub> and FE<sub>NH3</sub> over BTC/La-Co<sub>3</sub>O<sub>4-x</sub> NPs at -0.3 V vs. RHE for eight cycles.

with/without  $NO_3^-$  (Figure 3A). Within the current density curves, several spinodal or peaks are observed, indicative of three primary reactions designated as s1, S1, and S2.<sup>50,51</sup>

$s1:2^*H^+ + 2e^- \rightarrow H_2$	(Equation 1)
: $*NO_3^- + H_2O + 2e^- \rightarrow *NO_2^- + 2OH^-$	(Equation 2)
$*^*NO_2^- + 5H_2O + 6e^- \rightarrow NH_3 + 7OH^-$	(Equation 3)

S1

S2

Article

Upon the presence of NO<sub>3</sub><sup>-</sup>, the current densities drastically increase compared to that in the electrolyte without NO3<sup>-</sup>. Notably, BTC/La-Co3O4-x and Lav-Co3O4-x display higher current densities than pure Co<sub>3</sub>O<sub>4</sub>, suggesting the efficient eNO<sub>3</sub>RR activity of the electrocatalysts facilitated by the modification of La doping and BTC ligands (Figure S19). Additionally, all electrocatalysts demonstrate a consistent onset potential at 0.2 V vs. RHE during nitrate reduction. Within the potential range from -0.15 to -0.35 V vs. RHE, the peak labeled as S1 is attributed to the conversion from \*NO3 to \*NO2 through two PCET steps. Given the negligible contribution of HER within this potential range, the Tafel slopes have been extracted from Figure 3A to elucidate the reaction rate of \*NO3-to-\*NO2 conversion. As illustrated in Figure S20, the Tafel slopes of Co<sub>3</sub>O<sub>4</sub>, La-Co<sub>3</sub>O<sub>4-x</sub>, and BTC/La-Co<sub>3</sub>O<sub>4-x</sub> are determined to be 1,027.57, 288.79, and 278.87 mV decade<sup>-1</sup>, respectively. These findings illustrate the high concentration of  $O_v$  displays a higher capability for reducing \*NO<sub>3</sub> to  $*NO_2$ , which serve as active sites and provide abundant electrons for reducing nitrate. At the same time, the contribution of BTC ligands in this process is comparatively modest. The electrochemical impedance spectra provide further evidence of fast electron transfer attributed to La doping (Figure S21). As anticipated, the charge transfer resistance is markedly reduced for La-Co<sub>3</sub>O<sub>4-x</sub> (53.68  $\Omega$ ) and BTC/La- $Co_3O_{4-x}$  (46.42  $\Omega$ ) in comparison to pristine  $Co_3O_4$  NPs (66.34  $\Omega$ ). As the potential becomes progressively negative in the LSV curves, the peaks marked as S2 come to the forefront. These peaks correspond to the reduction from  $*NO_2^-$  to  $NH_3$ , continuing until the onset of HER. As is known, the eNO<sub>3</sub>RR involves several by-products, including  $NO_2^-$ ,  $NH_3$ , and hydrazine hydrate ( $N_2H_4$ ). The results of colorimetry highlight the  $NH_3$  and  $NO_2^-$  species as the principal products throughout the  $eNO_3RR$  process in this system, while the yield of N<sub>2</sub>H<sub>4</sub> is negligible. As depicted in Figure 2B, the La-doped samples significantly enhance the FE of  $NH_3$  (FE<sub>NH3</sub>) compared to pure  $Co_3O_4$ , particularly by diminishing the production of  $NO_2^{-}$ , which is consistent with the LSV results that the La-Co<sub>3</sub>O<sub>4-x</sub> has a fast \*NO<sub>3</sub>-to-\*NO<sub>2</sub> activity. Subsequent co-modification with BTC ligands further elevates the eNO3RR performance, demonstrating an outstanding  $FE_{NH3}$  of 99.41% at -0.3 V vs. RHE, surpassing that of La-Co<sub>3</sub>O<sub>4-x</sub> (91.77%) and Co<sub>3</sub>O<sub>4</sub> (63.44%). More importantly, such high FE<sub>NH3</sub> (>90%) could maintain at a broad potential range ( $-0.3 \sim -0.7$  V vs. RHE), whereas the  $FE_{NH3}$  for La-Co<sub>3</sub>O<sub>4-x</sub> and Co<sub>3</sub>O<sub>4</sub> distinctly declines. At high potentials, it is recognized that the two-electron transfer HER competes with the eight-electron transfer  $eNO_3RR$  (s1 region). Consequently, in most electrocatalysts, intensified hydrogen generation emerges as the potential becomes increasingly negative, impeding the eNO<sub>3</sub>RR selectivity.<sup>52,53</sup> However, the FE<sub>H2</sub> for BTC/La-Co<sub>3</sub>O<sub>4-x</sub> NPs is notably suppressed compared to the counterparts, keeping a low value below 10% (Figure 3C). The Tafel slopes of the HER, as seen in the inset, are derived from the s1 region in Figure 3A, of which the much bigger slope of BTC/ La-Co<sub>3</sub>O<sub>4-x</sub> (210.5 mV decade<sup>-1</sup>) means the inherently poor HER activity. This phenomenon is attributed to the constrained activity of free water around the active sites, which comes from establishing H-bonds between the carboxylate groups in BTC ligands and free water molecules. This bonding arrangement subsequently regulates the accessibility and kinetics of protons for the PCET steps and thus affects the selectivity of  $eNO_3RR$ . Under the high  $FE_{NH3}$  and selectivity, the BTC/La-Co<sub>3</sub>O<sub>4-x</sub> presents a higher partial current density and yield rate for  $NH_3$  (97.70 mA cm<sup>-2</sup> for  $j_{\rm NH3}$  and 31.24 mg h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup> for Y<sub>NH3</sub>) at -0.7 V vs. RHE, about 1.79/1.58 and 2.87/2.48 times higher than  $j_{NH3}/Y_{NH3}$  of La-Co<sub>3</sub>O<sub>4-x</sub> and Co<sub>3</sub>O<sub>4</sub>, respectively. The intrinsic activity of these catalysts is subsequently assessed by normalizing the electrochemically active surface area (ECSA; Figure S22). Remarkably, the ECSA-normalized current densities have the same trend as the unnormalized LSV curves, where BTC/La-Co<sub>3</sub>O<sub>4-x</sub> exhibits the highest activity among the measured potential range,

![](_page_9_Picture_3.jpeg)

![](_page_10_Picture_0.jpeg)

indicating the distinguished intrinsic activity for  $eNO_3RR$ . This performance is notably superior to state-of-the-art catalysts reported in the literature, particularly regarding the yield rate for NH<sub>3</sub> (Figure 3F; Table S3). In fact, its NH<sub>3</sub> synthesis rate ranks among the most NH<sub>3</sub>-synthesizing electrocatalysts, which is promising for large-scale NH<sub>3</sub> electrosynthesis.

To validate the fast \*NO<sub>3</sub>-to-\*NO<sub>2</sub> activity after La doping and the suppressed HER due to BTC ligands, we conduct a comparative electrochemical assessment in the electrolytes containing 0.05 M NO2- or 0.05 M NO3-, respectively. As shown in Figures S23 and S24, the higher current density and yield rate of NH<sub>3</sub> in electrochemical  $NO_2^-$  reduction reaction (eNO<sub>2</sub>RR) highlight the much easier reaction kinetics than eNO<sub>3</sub>RR. Accordingly, there is a big gap between the FE<sub>NH3</sub> for eNO<sub>2</sub>RR and eNO<sub>3</sub>RR of pure Co<sub>3</sub>O<sub>4</sub>, which suggests the reaction barrier during the conversion from \*NO<sub>3</sub> to \*NO<sub>2</sub>, that is, leading to the high yield rate of NO<sub>2</sub><sup>-</sup> as proved in Figure 3B. On the contrary, introducing La atoms into the  $Co_3O_4$  lattice distinctly narrows this difference. This effect is caused by the generated O<sub>v</sub> implementing abundant electron supply and faster electron transfer rate, overcoming the block during the \*NO<sub>3</sub>-to-\*NO<sub>2</sub> process. It is important to note that the FEs depicted in Figure S24 exhibit a distinctive volcanoshaped profile. However, for BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, the difference between eNO<sub>2</sub>RR and eNO<sub>3</sub>RR is minimal, and the volcano shape is comparatively subdued, particularly at more negative potentials, suggesting the suppressed HER. Consequently, it can be deduced that the high-rate eNO3RR performance observed in BTC/La-Co3O4-x is attributed to the coexistence of the synergistically generated O<sub>v</sub> and carboxylate groups in BTC ligands, in which the former catalyzes the reduction from \*NO<sub>3</sub> to \*NO $_2$  and the latter suppresses the competing HER, thereby contributing to the tandem catalysis of nitrate. In practical wastewater treatment, where polluted nitrate concentrations can vary from 0.88 mM to 1.95 M,<sup>54</sup> it is crucial to assess the performance of the electrolyte with different nitrate concentrations ([NO<sub>3</sub><sup>-</sup>]). As displayed in Figure S25, the  $Y_{NH3}$  climbs with the increasing [NO<sub>3</sub><sup>-</sup>] (5–500 mM) at –0.3 V vs. RHE. Remarkably, the FE<sub>NH3</sub> exceeds 70% at all the concentrations and 90% at the  $[NO_3^-]$ of 10-500 mM, indicating the promising potential of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> in eNO<sub>3</sub>RR for environmental applications. The slight reduction of FE<sub>NH3</sub> when the [NO<sub>3</sub><sup>-</sup>] surpasses 50 mM is more likely because of the deactivation of the active sites due to the sluggish transfer of generated NH<sub>3</sub>.<sup>18,55</sup> Additionally, the <sup>1</sup>H nuclear magnetic resonance (NMR) analysis is undertaken to confirm the origin of the nitrogen incorporated in the produced NH<sub>3</sub> (Figure S26). The absence of a peak in the <sup>1</sup>H NMR spectra prior to the nitrate reduction reaction is changed to the characteristic splitting modes in the spectra that measure the standard  ${}^{14}NH_4^+$  or  ${}^{15}NH_4^+$  electrolyte after  $eNO_3RR$ , proving all nitrogen in the generated  $NH_3$  comes from  $^{15}N$  isotope-labeled  $^{15}NO_3^{-1}$ or <sup>14</sup>N isotope-labeled <sup>14</sup>NO<sub>3</sub><sup>-</sup>. Moreover, the concentrations of detected <sup>15</sup>NH<sub>4</sub><sup>+</sup> of all the samples are closely similar to that measured by the UV-visible (UV-vis) method, which suggests the accuracy of the data obtained in this work. To estimate the electrochemical durability of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> for eNO<sub>3</sub>RR, we perform consecutive cycling tests at -0.3 V vs. RHE (Figure 3G). After eight cycles, both the yield rates and FEs of NH<sub>3</sub> product are well preserved, indicating excellent stability with a stable FE<sub>NH3</sub> exceeding 95% and  $Y_{NH3}$  beyond 5.50 mg h<sup>-1</sup> mg<sub>cat</sub><sup>-1</sup> over the cycles. The morphology and valence states of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> after the stability test also have no significant change (Figures S27 and S28).

### Mechanism study and computational insights into the eNO\_3RR on BTC/La-Co\_3O\_{4-x} NPs

To gain a comprehensive understanding of the underlying mechanism driving the enhanced  $eNO_3RR$  activity of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> NPs, we first perform DFT

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calculations to investigate the interaction between BTC ligands and water molecules. As delineated by the electrostatic potential (ESP) mapping (Figure 4A), a positive potential envelopes the H atoms in water, while a negative potential surrounds the O atoms in the COO<sup>-</sup> group of BTC ligands. This distribution indicates the inherent electrostatic interaction between them, constituting the formation of H-bonds (H ... O–H). Subsequently, the binding energy of water molecules to BTC ligands was computed to be -0.367 eV, thereby affirming the robustness of the H-bonding interaction.<sup>56</sup> Furthermore, the MD simulations were undertaken to explore the molecular behavior, including  $H_2O$  and  $NO_3^-$ , at the side of the interface from the electrolyte (Figures 4C and 4D). It could be found that water molecules are bonded with neighbor COO<sup>-</sup> by H-bonds in the simulated results (the enlarged photo in BTC/La-Co<sub>3</sub>O<sub>4-x</sub>). Notably, the presence of electrostatic mutual repulsion between the negatively charged COO<sup>-</sup> and NO<sub>3</sub><sup>-</sup> ions precludes the formation of H-bonds between them,  $5^{57}$  whereas this ensures enough NO<sub>3</sub><sup>-</sup> could be adsorbed by active sites for eNO<sub>3</sub>RR. After a simulation duration of 100 ns, a comparative analysis is made between the near-surface molecule behaviors of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, modified by BTC ligands, and the pure Co<sub>3</sub>O<sub>4</sub> catalyst. These results, as depicted in the concentration profile of Figure 4E, unveil a relatively low concentration of ions in the near-surface region of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, validating the constrained water activity due to the formation of H-bonds between water and COO<sup>-</sup> ligands. Besides, the results are the same when we place  $BTC/La-Co_3O_{4-x}$  and  $Co_3O_4$  in 1.0 M KOH solution without NO<sub>3</sub><sup>-</sup>, of which a higher concentration of H<sub>2</sub>O is observed at the interface of Co<sub>3</sub>O<sub>4</sub> (Figure S29). These computational findings collectively expound upon the reasons behind the limited proton accessibility of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> and its consequent lower FE<sub>H2</sub> during nitrate reduction. The limitation of proton accessibility influences the selectivity between  $H^+$  and  $NO_3^-$  for an active site, in which  $NO_3^-$  is preferentially adsorbed instead of H<sup>+</sup>, promoting the kinetics of  $eNO_3RR$ and suppressing HER. The MD simulations provide invaluable insights into the role of H-bonds and electrostatic interactions in shaping the behavior of these catalysts in nitrate reduction processes. Since BTC has three COO<sup>-</sup> groups, terephthalic acid (TPA) with two COO<sup>-</sup> groups is combined with La-Co<sub>3</sub>O<sub>4-x</sub> to study the eNO<sub>3</sub>RR performance (Figure S30). As anticipated, the current density observed with TPA/La-Co<sub>3</sub>O<sub>4-x</sub> exhibits a marginal reduction compared to that of BTC/La- $\rm Co_3O_{4\text{-}x}$  and achieves a higher  $\rm FE_{NH3}$  of 97.84% at -0.4 V vs. RHE and  $\rm Y_{NH3}$  of 23.73 mg  $h^{-1}$  mg<sub>cat</sub><sup>-1</sup> at -0.7 V vs. RHE. The superior but lower performance of TPA/La-Co<sub>3</sub>O<sub>4-x</sub> compared to BTC/La-Co<sub>3</sub>O<sub>4-x</sub> suggests the pivotal role of carboxylic groups in the organic ligands as the efficient functional component enhancing the eNO<sub>3</sub>RR rate. Concurrently, the greater number of carboxylic groups in BTC leads to a more remarkable eNO<sub>3</sub>RR performance than TPA. To offer a clearer understanding of the diffusion behaviors of  $NO_3^-$  and  $H_2O$ , a schematic is depicted in Figure 4F. During the eNO<sub>3</sub>RR process, the La-doped Co<sub>3</sub>O<sub>4</sub> surface demonstrates a propensity for facile adsorption of  $NO_3^-$  ions through interaction with  $O_v$  sites. Conversely, H<sub>2</sub>O molecules encounter hindrance due to the presence of COO<sup>-</sup> ligands on BTC, which gives rise to the formation of H-bonds. The confined transfer channels for H<sub>2</sub>O limit the accessibility of protons to active sites; meanwhile, the electrostatic mutual repulsion between COO<sup>-</sup> and NO<sub>3</sub><sup>-</sup> further ensures the preferential adsorption of NO3<sup>-</sup> ions. After that, the water bonded by H-bonds supplies protons to intermediates adsorbed on active sites and motivates PCET steps in  $eNO_3RR$ , eventually generating NH<sub>3</sub>. Therefore, this phenomenon decreases the competing HER and significantly promotes the selectivity of eNO<sub>3</sub>RR.

After the simulation, we use the *in situ* thin-layer FTIR spectrum to track intermediate species within a thin electrolyte layer above the surface of catalysts during the

![](_page_11_Picture_4.jpeg)

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Figure 4. Simulating calculations and electrochemical in situ FTIR spectra

(A) Electrostatic potential (ESP) mapping of H<sub>2</sub>O, BTC ligand, and BTC ligand with H<sub>2</sub>O molecules.

- (B) Calculated binding energy of the H-bond between water and BTC molecule.
- (C) Molecular dynamics simulation of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> in 1.0 M KOH solution + 10 mM KNO<sub>3</sub>.
- (D) Molecular dynamics simulation of  $Co_3O_4$  in 1.0 M KOH solution + 10 mM KNO<sub>3</sub>.
- (E) Distribution of  $H_2O + NO_3^-$  along the z axis electrode distance based on molecular dynamics simulation.
- (F) The schematic diffusion behaviors of  $NO_3^-$  and  $H_2O$  on the surface of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> electrode.
- (G) Electrochemical thin-layer in situ FTIR spectra of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> during eNO<sub>3</sub>RR.
- (H) Electrochemical thin-layer in situ FTIR spectra of Co<sub>3</sub>O<sub>4</sub> during eNO<sub>3</sub>RR.
- (I) Calculated  $I_{\rm NH4+}/(I_{\rm NH4+}$  +  $I_{\rm H2O})$  ratios from in situ FTIR spectra.
- (J) Calculated  $I_{\rm NO2-}/(I_{\rm NO2-}$  +  $I_{\rm NH2OH})$  ratios from in situ FTIR spectra.
- (K) Electrochemical in situ ATR-SEIRAS spectra of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, La-Co<sub>3</sub>O<sub>4-x</sub>, and Co<sub>3</sub>O<sub>4</sub>, respectively.

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reaction, which will bring in-depth insights into eNO<sub>3</sub>RR mechanisms. Herein, a reference spectrum (R<sub>ref</sub>) is established at a potential of 0.9 V, and working spectra (R<sub>s</sub>) are then obtained along with the potentials increased at an interval of 0.1 V. The acquired FTIR spectra are displayed as relative changes in the reflectance, denoted as  $\Delta R/R = (R_S - R_{ref})/R_{ref}$ . <sup>51</sup> Consequently, the peaks ascending in FTIR spectra mean the consumption of reactants, including  $NO_3^-$  and  $H_2O$ , while the downward peaks correspond to the emergence of intermediates and resultant products, such as NO<sub>2</sub><sup>-</sup>. Accordingly, in Figures 4G, 4H, and S31, six distinct absorption bands stand out, centered at 1,157, 1,226, 1,326, 1,365, 1,427, and 1,650 cm<sup>-1</sup>, respectively. Firstly, the upward bands located at 1,326 and 1,365 cm<sup>-1</sup> are attributed to the N–O asymmetric stretching vibration of  $NO_3^-$ , which occurs obviously after the potential surpasses 0.3 V, close to the onset potential in Figure 3A, indicating the beginning of nitrate reduction.<sup>58</sup> Besides, three downward bands around 1,157, 1,226, and 1,427 cm<sup>-1</sup> are ascribed to -N-O- stretching vibration of intermediate hydroxylamine (NH<sub>2</sub>OH), N–O antisymmetric stretching vibration of  $NO_2^-$  and N– H bending mode of  $NH_4^+$  species, respectively, <sup>18,59,60</sup> demonstrating the generated  $NO_2^-$  from reducing  $NO_3^-$  and the following reduction by-products of  $NH_2OH$ , eventually leading to the final products of NH<sub>3</sub>. Finally, the upward FTIR bands centered at 1,650 cm<sup>-1</sup> are related to water electrolysis, a phenomenon responsible for hydrogeneration leading to  $NH_3$  evolution after deoxygenation. The evident decreased water activity in BTC/La-Co<sub>3</sub>O<sub>4-x</sub> illustrates the existence of H-bonds. To better understand the relationship between different reactants and products, we calculate the  $I_{\rm NH4+}/(I_{\rm NH4+}$  +I\_{\rm H2O}) and  $I_{\rm NO2-}/(I_{\rm NO2-}$  +I\_{\rm NO2-+NH2OH}) ratios ("I" means intensity) from in situ FTIR spectra. As is known, both HER and eNO3RR processes necessitate \*H originating from water electrolysis; thereby, the high I<sub>H2O</sub> accelerates the hydrogeneration essential for eNO<sub>3</sub>RR and expedites hydrogen evolution. Drawing from the earlier discussion, it is clear that BTC ligands restrain water activity and suppress HER by forming H-bonding between H<sub>2</sub>O molecules and COO<sup>-</sup>. Therefore, the I<sub>NH4+</sub>/(I<sub>NH4+</sub> + I<sub>H2O</sub>) ratio could provide support in clarifying the proportion of consumed \*H in these two competing reactions and demonstrating the NH<sub>3</sub> selectivity of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> and Co<sub>3</sub>O<sub>4</sub> (Figure 4I; Table S4). It was found that the ratio of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> is significantly higher than that of  $Co_3O_4$ , which suggests that much more \*H is being used to generate NH<sub>4</sub><sup>+</sup> rather than H<sub>2</sub> during eNO<sub>3</sub>RR, indicating the good NH<sub>3</sub> selectivity in BTC/La-Co<sub>3</sub>O<sub>4-x</sub> and also proving the advantageous role of organic BTC ligands in suppressing competing HER. Furthermore, it becomes apparent that the  $v(NH_2OH)$  bands manifest after the formation of  $v(NO_2^-)$  bands. This pattern indicates the gradually faster conversion from NO<sub>2</sub><sup>-</sup> to NH<sub>2</sub>OH through hydrodeoxidation, encompassing crucial steps such as the transition from  $NO_2^-$  to  $*NO_2$  and the ensuing hydrogeneration process by increased applied potential. Therefore, the comparison in band intensity of  $NO_2^-$  relative to the collective intensity of  $NO_2^-$  and  $NH_2OH [I_{NO2-}/(I_{NO2-} + I_{NH2OH})]$ serves as a visual indicator of the conversion rate from NO<sub>2</sub><sup>-</sup> to NH<sub>2</sub>OH via hydrodeoxidation. The various ratios of the samples exhibit a consistent declining trend as the applied potential increases in Figure 4J and Table S5. Interestingly, BTC/La-Co<sub>3</sub>O<sub>4-x</sub> and La-Co<sub>3</sub>O<sub>4-x</sub> have similar slopes, yet they are notably steeper when compared to  $Co_3O_4$ . This observation confirms the significant impact of La doping-induced  $O_{v_1}$ proving the role in facilitating the gradual reduction from NO<sub>2</sub><sup>-</sup> to the following products, such as NH<sub>2</sub>OH. More importantly, the lowest ratios of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> suggest the best  $eNO_3RR$  performance among the samples. In Figure 4K, the ATR-SEIRAS spectra, which have bands ranging from 2,078 to 2,113 cm<sup>-1</sup>, can be observed, representing original metal-H-bonds influenced by the Stark effect.<sup>61-64</sup> Interestingly, an increased trend of metal-H (Co-H)-bonding emerges as the order of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, La-Co<sub>3</sub>O<sub>4-x</sub>, and Co<sub>3</sub>O<sub>4</sub> at the same potential. This effect points to much

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![](_page_14_Figure_3.jpeg)

#### Figure 5. Reaction pathway during eNO<sub>3</sub>RR over BTC/La-Co<sub>3</sub>O<sub>4-x</sub>

(A) Differential electrochemical mass spectrometry (DEMS) measurements of eNO<sub>3</sub>RR on BTC/La-Co<sub>3</sub>O<sub>4-x</sub>.
(B) *In situ* Raman spectra of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> during eNO<sub>3</sub>RR at different potentials in a mixed solution (0.1 M KOH + 50 mM KNO<sub>3</sub>).

(C) Corresponding contour plots from  $1,100 \text{ cm}^{-1}$  to  $1,400 \text{ cm}^{-1}$  in (B).

(D) The proposed structural models represent various intermediates and proton transfer mediators on  $BTC/La-Co_3O_4$  during the pathway of  $eNO_3RR$ . The red, dark blue, and green balls represent O, N, and H atoms that participate in the  $eNO_3RR$ .

less \*H adsorption on the surface of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, which means more NO<sub>3</sub><sup>-</sup> adsorbed on active sites and the fast consumption of \*H. Moreover, the higher wavenumbers associated with Co–H-bonds in Co<sub>3</sub>O<sub>4</sub> validate their enhanced \*H-bonding capacity.<sup>65</sup> According to the analysis of *in situ* FTIR measurement, it can be concluded that the coexistence of induced O<sub>v</sub> and COO<sup>-</sup> organic ligands within BTC/La-Co<sub>3</sub>O<sub>4-x</sub> not only expedites the conversion of \*NO<sub>3</sub><sup>--</sup>\*NO<sub>2</sub>-NH<sub>2</sub>OH but also suppresses the competitive HER process, limiting proton accessibility. This interplay culminates in a remarkable eNO<sub>3</sub>RR performance characterized by high activity and selectivity.

To construct a comprehensive description of the reaction pathway of BTC/La- $Co_3O_{4-x}$  during eNO<sub>3</sub>RR, online DEMS was carried out for five subsequent LSV scan cycles (each cycle involves a scan from 0.5 to -0.7 V vs. RHE) to detect the intermediate species generated during the eNO<sub>3</sub>RR. As depicted in Figure 5A, the mass-to-charge ratio (m/z) signals at 17, 30, 33, and 46 are detected via online DEMS, aligning with the identification of corresponding products: NH<sub>3</sub>, NO, NH<sub>2</sub>OH, and NO<sub>2</sub>, respectively.<sup>66</sup> Notably, the detection of NH<sub>2</sub>OH is of particular significance, as its presence is also tracked within the *in situ* FTIR spectra illustrated in

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Figure 4G. This concurrent occurrence suggests the hydrodeoxidation pathway in this system follows the trajectory from \*NO<sub>2</sub> to \*NH<sub>2</sub>OH. Furthermore, the investigation extends to in situ Raman spectra acquired from BTC/La-Co<sub>3</sub>O<sub>4-x</sub> in a solution containing  $NO_3^-$  (Figure 5B). Besides the Raman peaks associated with  $-COO^$ and -COOH functionalities, additional bands have been attributed to three distinct groups:  $NO_3^-$  vibrations (1,047 cm<sup>-1</sup>) and adsorbed  $NO_3^-$  species (1,013 and 1,372 cm<sup>-1</sup>), generated NO<sub>2</sub><sup>-</sup> vibrations (1,324 cm<sup>-1</sup>) and adsorbed NO<sub>2</sub><sup>-</sup> species  $(1,198 \text{ cm}^{-1})$ , and generated NH<sub>3</sub> vibrations  $(1,142 \text{ and } 1,495 \text{ cm}^{-1})$ .<sup>67</sup> To facilitate a more comprehensive understanding of these diverse intermediates, a corresponding contour plot ranging from 1,100  $\text{cm}^{-1}$  to 1,400  $\text{cm}^{-1}$  is depicted in Figure 5C, derived from the data showcased in Figure 5B. As anticipated, the bands associated with adsorbed NO<sub>3</sub><sup>-</sup> and generated NH<sub>3</sub> appear after open-circuit potential (OCP), and their intensities gradually increase as the potential becomes more negative, indicating the more active eNO3RR on BTC/La-Co3O4-x. More importantly, the bands for producing NO<sub>2</sub> are detected from the potential range from 0.15 to -0.15 V vs. RHE, consistent with the experimental results, but they disappear upon the appearance of adsorbed  $NO_2^-$  signals, which are discovered from -0.10to -0.25 V vs. RHE, suggesting the gradually increasing capacity for adsorbing dissociative  $NO_2^-$  ions over BTC/La-Co<sub>3</sub>O<sub>4-x</sub>. Furthermore, the adsorbed  $NO_2^$ band vanishes after the potential drops below -0.25 V vs. RHE, coinciding with a conspicuous enhancement in the Raman peak corresponding to NH<sub>3</sub>. These observations validate the outstanding capacity of BTC/La-Co<sub>3</sub>O<sub>4-x</sub> to convert \*NO<sub>3</sub> to \*NO<sub>2</sub> to NH<sub>3</sub>, underscoring its remarkable efficacy in facilitating the eNO<sub>3</sub>RR process. Incorporating the insights garnered from DEMS and in situ Raman studies, we propose the possible eNO<sub>3</sub>RR pathway and calculate the Gibbs free energy of each intermediate on BTC/La-Co<sub>3</sub>O<sub>4-x</sub> and the counterparts at different pH values by DFT (Figures 5D and S32-S35). In addition to the adsorption and desorption of NO<sub>3</sub><sup>-</sup> and NH<sub>3</sub>, respectively, the pathway involves a total of nine PCET steps during eNO3RR, including the hydrodeoxidation process of \*NO3-\*NO2OH-\*NO2-\* NOOH-\*NO, as well as the hydrogenation procedures of \*NO-\*NHO-\*NH<sub>2</sub>O-\* NH<sub>2</sub>OH-\*NH<sub>2</sub>-\*NH<sub>3</sub>. As shown in Figure S32, the initial upward trend (0.25 eV) from  $NO_3^-$  to \*NO<sub>3</sub> suggests an energetically unfavorable reaction of adsorbing  $NO_3^-$  over  $Co_3O_4$ , whereas it converts to downward trend (-0.33 eV for La- $Co_3O_{4-x}$  and -0.48 eV for BTC/La-Co<sub>3</sub>O<sub>4-x</sub>) upon doping La atoms, indicating the easier adsorption of  $NO_3^-$  on the  $O_v$  site in La-Co<sub>3</sub>O<sub>4-x</sub>, which are also proved by the much more favorable  $NO_3^-$  adsorption energy on the  $O_v$  site compared to the Co site of La-Co<sub>3</sub>O<sub>4-x</sub> (Figure S36). The projected density of states (PDOS) clearly demonstrates the stronger hybridization between the O 2p orbital in NO3<sup>-</sup> and the 3d orbital of the Co atom in BTC/La-Co $_3O_{4-x}$  (Figure S37). In the meantime, in both acidic and alkaline environments (pH values are 0 and 14, respectively), La-Co<sub>3</sub>O<sub>4-x</sub> and BTC/La-Co<sub>3</sub>O<sub>4-x</sub> exhibit a reduced uphill free energy change (\*NO<sub>3</sub>-\*NO<sub>2</sub>OH) in the next PCET reaction, coupled with a higher NO<sub>2</sub><sup>-</sup> desorption capacity. The enhanced affinity of  $*NO_2^-$  species prevents its desorption from generating  $NO_2^-$  by-product during reduction, significantly accelerating the conversion from  $*NO_3$  to  $*NO_2$ . More importantly, the rate-determining step (RDS) is the conversion from \*NO to \*NHO. For BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, the RDS exhibits a notably smaller energy barrier than that of La-Co<sub>3</sub>O<sub>4-x</sub> and Co<sub>3</sub>O<sub>4</sub>. This finding reflects the unique advantages of functional organic ligands compared to organic additives. That is, in addition to controlling proton accessibility, they can also regulate the local electronic environment around the active site to change the adsorption energy of various intermediates. Combining the above results, we proposed the structural models representing various intermediates and proton transfer mediators to give a straightforward understanding of the reaction pathway and PCET mechanisms

![](_page_15_Picture_3.jpeg)

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(Figure 5D). The key factor is the contribution of free H<sub>2</sub>O molecules originating from the bulk electrolyte. These molecules undergo a sequence of interactions: initially, they engage in H-bonds with coordinatively unsaturated interfacial COO<sup>-</sup> sites from organic ligands, effectively preventing the direct adsorption of H<sub>2</sub>O on active sites and suppressing HER. In the subsequent step (ii), an H atom from the bonded  $H_2O$  joins with an O atom from \*NO<sub>3</sub>, facilitated by the provision of electrons from generated O<sub>v</sub>, culminating in a complete PCET process. Simultaneously, the remaining -OH is released into the bulk electrolyte due to electrostatic repulsion forces between OH<sup>-</sup> and COO<sup>-</sup>, thereby ensuring enough COO<sup>-</sup> that could bond with free  $H_2O$ . This sequence unfolds across each PCET step, effectively controlling the proton accessibility but not blocking them from participating in hydrogenation for the intermediates on active sites, giving a decisive contribution to the enhancement of eNO<sub>3</sub>RR selectivity of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>. Based on the results discussed above, we get a comprehensive description of the reaction pathway of the samples in this work. Herein, through a synergistic interplay of generated O<sub>v</sub> resulting from La doping and COO<sup>-</sup> groups in combined carboxylic-based organic ligands, the increment of eNO<sub>3</sub>RR performance is achieved. The induced O<sub>v</sub> acts as active sites for adsorbing NO<sub>3</sub><sup>-</sup> while redistributing electrons and promoting the electron transfer to the PCET steps, making faster \*NO<sub>3</sub>-to-\*NO<sub>2</sub> conversion and reducing the generated  $NO_2^-$  side-product. In tandem, the H-bonds formed between H<sub>2</sub>O and COO<sup>-</sup> lead to indirect proton accessibility to active sites in every PCET step, not only balancing the adsorption between \*H and \*NO<sub>3</sub> species but also lowering the energy barrier of RDS (\*NO to \*NHO), thus suppressing the competing HER and boosting both the selectivity and activity of eNO<sub>3</sub>RR.

#### Conclusions

In summary, we designed an electrocatalyst of  $Co_3O_4$  NPs modified with doped La atoms and COO<sup>-</sup>-based organic ligands. This innovative catalyst design has elucidated the significant synergistic effect of induced oxygen vacancies due to La doping and functionalized COO<sup>-</sup> organic ligands on facilitating the nitrate adsorption, confining the water activity, and regulating the PCET steps in nitrate reduction. This BTC/La-Co<sub>3</sub>O<sub>4-x</sub> electrocatalyst exhibited high activity and selectivity during eNO3RR, achieving an FE as high as 99.41% with an ammonia yield rate of 5.62 mg  $h^{-1}$  mg<sub>cat</sub><sup>-1</sup> at -0.3 V vs. RHE. Notably, the catalyst sustains NH<sub>3</sub> production with >90% FE within a wide potential window (400 mV, from -0.3 to -0.7 V vs. RHE), which is top ranked among the electrocatalysts for eNO<sub>3</sub>RR so far. The proposed reaction mechanism combines the results of in situ FTIR, in situ Raman, MD simulations, and DFT calculations. In detail, La doping provides abundant active sites (oxygen vacancies) for adsorbing NO<sub>3</sub><sup>-</sup> and significantly lowers the energy barrier of \*NO<sub>3</sub>-to-\*NO<sub>2</sub> steps, which are beneficial from electron redistribution. Also, the COO<sup>-</sup> can form H-bonds with free water, thereby confining the water activity and leading to the controlled proton accessibility to active sites and regulated hydrogenation PCET steps, which plays a decisive contribution to the enhancement of selectivity of eNO<sub>3</sub>RR. This work provides a rational strategy based on carboxylic organic ligands for a high ammonia production rate. It can contribute to subsequent catalyst optimization and scale-up for applications across diverse electrochemical techniques, particularly those where the HER poses a competing challenge, such as CO<sub>2</sub> reduction.

#### **EXPERIMENTAL PROCEDURES**

#### **Resource** availability

#### Lead contact

Requests for further information and resources should be directed to and will be fulfilled by the lead contact, Prof. Johnny C. Ho (johnnyho@cityu.edu.hk).

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![](_page_17_Picture_2.jpeg)

#### Materials availability

All catalysts generated in this study will be made available upon request, but we may require a payment and/or a completed materials transfer agreement.

#### Data and code availability

All data related to this study included in the article and supplemental information will be provided by the lead contact, Prof. Johnny C. Ho (johnnyho@cityu.edu.hk), upon reasonable request.

#### Preparation of Co<sub>3</sub>O<sub>4</sub> NPs

The Co<sub>3</sub>O<sub>4</sub> NPs were prepared via a facile coprecipitation method. Typically, 0.25 mM cobalt nitrate hexahydrate (Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, Sigma-Aldrich) was dissolved into 25 mL of deionized (DI) water. After vigorous stirring for 1 h, 25 mL of 0.375 M NaOH solution was slowly dropwise into the Co(NO<sub>3</sub>)<sub>2</sub> precursor solution. After further stirring for 2 h, the precipitate was washed with DI water and ethyl alcohol several times and collected by centrifugation, followed by vacuum drying at 60°C overnight. The resulting cakes were crushed into fine powder in a mortar and then calcined in air at 500°C for 5 h.

#### Preparation of La<sub>v</sub>-Co<sub>3</sub>O<sub>4-x</sub>, where y represents the atom % of La

For La<sub>y</sub>-Co<sub>3</sub>O<sub>4-x</sub>, 5, 15, and 25 mg of La(NO<sub>3</sub>)<sub>3</sub>·6H<sub>2</sub>O (Sigma-Aldrich) were added into the Co(NO<sub>3</sub>)<sub>2</sub> precursor solution, respectively. The subsequent procedures were the same as preparing Co<sub>3</sub>O<sub>4</sub> NPs. The atom % of La were determined to be 3.02, 6.29, and 9.11 atom % by inductively coupled plasma emission spectrometry (ICP-OES), which were named as La<sub>3</sub>-Co<sub>3</sub>O<sub>4-x</sub>, La<sub>6</sub>-Co<sub>3</sub>O<sub>4-x</sub> and La<sub>9</sub>-Co<sub>3</sub>O<sub>4-x</sub>, respectively.

#### Preparation of BTC/La-Co<sub>3</sub>O<sub>4-x</sub>

Herein, La<sub>9</sub>-Co<sub>3</sub>O<sub>4-x</sub> was chosen as a sample for combining with BTC ligands, abbreviated here as La-Co<sub>3</sub>O<sub>4-x</sub>. In detail, 5 mg of H<sub>3</sub>BTC (Sigma-Aldrich) and 50 mg of La-Co<sub>3</sub>O<sub>4-x</sub> were mixed with 20 mL of dimethylformamide (DMF, Sigma-Aldrich), followed by stirring for 2 h. Finally, the precipitate was washed and centrifuged several times with fresh DMF, ethyl alcohol, and DI water, followed by vacuum drying at 60°C overnight.

#### Characterization

Scanning electron microscopy (SEM; FEI Quanta 450 FESEM), transmission electron microscopy (TEM; Tecnai G2 20), HRTEM (Tecnai G2 20), and SAED were used to observe the micromorphology and elemental distribution of the catalysts. XRD patterns were collected using a Bruker D8 Advance powder diffractometer to investigate the phase structures. XPS analyses using a Thermo Fisher ESCALAB XI+ system with an Al-Ka X-ray source (hv = 1,486.6 eV) was used to determine the elemental composition and valence state. All XPS spectra were corrected with a C 1s spectral line of 284.8 eV. ICP-OES (Agilent 730es) was carried out to determine the chemical composition of the catalysts. The electrolytes after electro-reduction were analyzed by UV-vis spectroscopy (Hitachi UH4150 UV-vis-NIR Spectrophotometer). To determine the origin of the ammonia produced, isotope labeling experiments were conducted on a Bruker 400MHz AVANCE III Nuclear Magnetic Resonance System (NMR-400). Zeta potential was determined by SurPASS 3 from Anton Paar in Austria in an aqueous solution (pH = 7). FTIR spectroscopy was recorded on a PerkinElmer FTIR Spectrometer. The XANES and the EXAFS analyses were investigated using the Singapore Synchrotron Light Source (SSLS) at the National University of Singapore. The sample was measured in transmission mode using La<sub>2</sub>O<sub>3</sub> as a reference sample. All X-ray absorption fine structure (XAFS) spectra were processed using the IFEFFIT package. Data reduction, data analysis,

![](_page_18_Picture_0.jpeg)

and EXAFS fitting were conducted using the Athena and Artemis programs from the Demeter data analysis packages, which utilize the FEFF6 program for EXAFS data fitting.<sup>68,69</sup> The energy calibration of the sample was conducted through standard, which as a reference was simultaneously measured. A linear function was subtracted from the pre-edge region, then the edge jump was normalized using Athena software. The  $\chi(k)$ data were isolated by subtracting a smooth, third-order polynomial approximating the absorption background of an isolated atom. The  $k^3$ -weighted  $\chi(k)$  data were Fourier transformed after applying a HanFeng window function ( $\Delta k = 1.0$ ). For EXAFS modeling, the global amplitude EXAFS (CN, R,  $\sigma^2$ , and  $\Delta E_0$ ) was obtained by nonlinear fitting, with least-squares refinement, of the EXAFS equation to the Fourier transformed data in R space, using Artemis software, the amplitude reduction factor  $S_0^2$  value (0.900) was set in the EXAFS analysis to determine the coordination numbers (CNs) in the La-O and La-Co scattering path in sample. For wavelet transform analysis, the  $\chi(k)$  exported from Athena was imported into the Hama Fortran code. The parameters were listed as follows: R range, 0–6 Å; k range, 0–16.0 Å-1; k weight, 3; and Morlet function with  $\kappa$  = 8,  $\sigma$  = 1 was used as the mother wavelet to provide the overall distribution.<sup>70</sup>

#### **Electrochemical characterization**

All the electrochemical measurements were carried out with an electrochemical workstation of Gamry G300 potential station at room temperature in an H-type electrolytic cell separated by a Nafion 117 membrane (DuPont). The anode chamber contained 50 mL of 0.1 M KOH electrolyte, while the cathode chamber contained 50 mL of 0.1 M KOH electrolyte with 0.05 M NO<sub>3</sub><sup>-</sup>. High-purity argon gas was bubbled into the cathodic chamber during electro-reduction to prevent possible side-competitive reactions such as the nitrogen reduction reaction (NRR). To prepare working electrodes, 5 mg of catalysts was dispersed in 960  $\mu$ L of solution with DI water and ethanol (3:1, v/v), followed by the addition of 40  $\mu$ L of Nafion solution. After sonicating for 1 h to form well-mixed inks, 50  $\mu$ L of ink was drop-casted on carbon cloth (CC; 1 × 1 cm) to attain a working electrode with a loading of 0.25 mg cm<sup>-2</sup>. In the three-electrode system, the catalysts on CC were used as working electrodes and a piece of Pt and Ag/AgCl (saturated KCl electrolyte) represented the counter and reference electrodes, respectively.

The LSV curves were recorded by a scan rate of 5 mV s<sup>-1</sup>. Electrochemical impedance spectroscopy (EIS) was obtained in the frequency range from 0.01 Hz to 100 kHz upon an alternating current (AC) voltage amplitude of 5 mV. The cyclic voltammetry curves were measured in a potential window where no Faradaic process occurred at different scanning rates (10–80 mV s<sup>-1</sup>) to determine the electrochemical double-layer capacitance (C<sub>dl</sub>). For eNO<sub>3</sub>RR experiments, potentiostatic tests were conducted for 1 h at different potentials with a magnetic stirring rate of 300 rpm. To ensure data accuracy, each catalyst was prepared for three samples for testing three times to get the error bar. All potentials were adjusted to the RHE using Equation 4:

#### $E(vs. RHE) = E(vs. Ag / AgCl) + 0.059 \times pH + 0.197 V$ (Equation 4)

#### Electrochemical in situ Raman spectroscopy analysis

*In situ* Raman spectra were collected on the WITec alpha300 R Raman System with an excitation wavelength of 532 nm. The working electrodes were cut to a plate shape with a diameter of 1 cm and put into the Raman cell with a quartz window. A platinum wire and Ag/AgCl served as the counter and reference electrodes, respectively. The Raman spectra were obtained at different potentials under control by an electrochemical workstation in the electrolyte of Ar-saturated 0.1 M KOH with 0.05 M KNO<sub>3</sub>. Each spectrum was an average of five continuously acquired spectra with a collection time of 30 s.

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![](_page_19_Picture_2.jpeg)

#### Electrochemical in situ FTIR reflection analysis

Electrochemical thin-layer in situ FTIR reflection spectroscopy was performed on a Nicolet iS50 spectrometer equipped with an mercury-cadmium-telluride (MCT) detector at different potentials controlled by an electrochemical workstation CHI760E. In detail, the catalyst ink was loaded on a glassy carbon electrode as a working electrode and pressed vertically on the CaF<sub>2</sub> window plate. There was a thin electrolyte (0.1 M KOH with 0.05 M KNO3) layer with a thickness of about 10  $\mu m$  between the glassy carbon electrode and  $CaF_2$  plate. Ar was used to purge the dissolved  $O_2$ and N<sub>2</sub> from the electrolyte. A platinum foil and an Ag/AgCl electrode were used as the counter and reference electrodes, respectively. The spectra were collected at different potentials (from 0.9 to -0.6 V vs. RHE) with an interval of 0.1 V. Reference spectra were collected at 0.9 V vs. RHE. Attenuated total reflection surfaceenhanced infrared absorption spectroscopy (ATR-SEIRAS) was also performed using a Nicolet iS50 spectrometer. Different from thin-layer FTIR experiments, the catalyst ink was dropped on a silicon crystal chemically deposited by a thin gold film. The incoming infrared beam has an angle of ca. 65° with the normal electrode surface. The spectra were collected at different potentials (from 0.4 to -0.4 V vs. RHE) with an interval of 0.05 V.

#### **Online DEMS measurements**

The online DEMS system consists of an electrochemical workstation and a mass spectrometer. The sampling probe of the mass spectrometer faces the working electrode of the electrochemical cell. Online DEMS measurement was performed on a homemade electrochemical cell with an electrolyte of 0.1 M KOH and 0.05 M  $NO_3^-$  equipped with a peristaltic pump. Ar was constantly bubbled into the electrolyte before and during the DEMS measurements. The system was controlled by an electrochemical workstation (CHI760E) with three electrodes: a glassy carbon electrode coated with BTC/La-Co<sub>3</sub>O<sub>4-x</sub> NPs electrocatalysts, Pt wire, and saturated Ag/ AgCl electrode were used as the working electrode, the counter electrode, and the reference electrode, respectively. The glassy carbon electrode was inserted from the bottom of the electrochemical cell. During the eNO<sub>3</sub>RR, the electrolyte flows into the thin layer in front of the electrode. Then, it flows into the detection cell through the capillaries, where the volatile chemicals can reach the detector through the Teflon membrane. LSV technology was employed from 0.5 to -0.7 V vs. RHE at a scan rate of 2 mV s<sup>-1</sup> for five cycles.

#### **Determination of products**

#### $NH_3$

The concentration of NH<sub>3</sub> was quantified by the indophenol blue method.<sup>71</sup> The electrolytes after electrolysis for 1 h were first removed from the electrochemical cell and diluted to the detection range. Then 2 mL of diluted electrolyte was taken out into a test tube, followed by adding 2 mL of solution A, which was prepared by mixing 5.0 wt % salicylic acid ( $C_7H_6O_3$ ) and 5.0 wt % sodium citrates ( $C_6H_5Na_3O_7 \cdot 2H_2O$ ) into 1.0 M NaOH solution. Then, 1 mL of solution B (diluted Na-CIO solution with a concentration of 0.05 M) was added to the above solution, followed by adding 0.2 mL of solution C (1.0 wt % sodium nitroferricyanide, Na<sub>2</sub>[Fe(NO)(CN)<sub>5</sub>]  $\cdot 2H_2O$ ). The test tube was placed on the test tube rack and stood for 2 h in a dark place under ambient conditions. The absorption spectrum of the solution was measured by UV-vis spectrophotometry, then the absorbance value was collected at a wavelength of 655 nm. The concentration-absorbance calibration curve of NH<sub>3</sub> was plotted by measuring the absorbance values of a series of standard NH<sub>4</sub>Cl solutions of known concentration dissolved in 0.1 M KOH.

![](_page_20_Picture_0.jpeg)

![](_page_20_Picture_1.jpeg)

#### $NO_2^-$

The concentration of NO<sub>2</sub> was quantified using the Griess method.<sup>72</sup> After electrolysis for 1 h, the electrolytes were first removed from the electrochemical cell and diluted to the detection range. A 5-mL diluted electrolyte was removed into a test tube, and 0.1 mL of color reagent was added. The color agent was prepared as follows: 50 mL of DI water and 10 mL of phosphoric acid were mixed together, followed by adding 4.0 g of *p*-aminobenzenesulfonamide and 0.2 g of N-(1-naphthyl)-ethylenediamine dihydrochloride. The mixture was then poured into a 100-mL volumetric flask and diluted to the calibration tail. The test tubes were then shaken, put in a test tube rack, stood for 20 min under ambient conditions, the solution's absorption spectrum measured with a UV-vis spectrophotometer, and the absorbance value collected at a wavelength of 540 nm. The concentration-absorbance calibration curve was plotted by measuring the absorbance values of a series of standard KNO<sub>2</sub> solutions of known concentration dissolved in 0.1 M KOH.

#### $N_2H_4$

The concentration of N<sub>2</sub>H<sub>4</sub> was quantified by Watt and Chrisp's method.<sup>73</sup> Two milliliters of diluted electrolyte was taken out into a test tube, followed by adding 2 mL of color reagent, which contains 5.99 g of p-(dimethylamino)benzaldehyde, 30 mL of concentrated HCl, and 300 mL of ethanol The test tubes were then shaken, put in a test tube rack, stood for 30 min under ambient conditions, the solution's absorption spectrum measured with a UV-vis spectrophotometer, and the absorbance value collected at a wavelength of 460 nm. The concentration-absorbance calibration curve was plotted by measuring the absorbance values of a series of concentrations known as standard N<sub>2</sub>H<sub>4</sub> solutions dissolved in 0.1 M KOH.

#### Isotope labeling experiment

The isotope labeling experiments were recorded by Bruker 400MHz AVANCE III Nuclear Magnetic Resonance System (NMR-400) using maleic acid ( $C_4H_4O_4$ ) as the internal standard. The nitrate reduction experiments were the same as usual, other than replacing K<sup>14</sup>NO<sub>3</sub> with K<sup>15</sup>NO<sub>3</sub> (98.5 atom%) as the feeding N-source for the isotopic label. Specifically, the obtained electrolytic electrolyte containing <sup>15</sup>NH<sub>4</sub><sup>+-15</sup>N was removed and adjusted to weak acid with 4 M H<sub>2</sub>SO<sub>4</sub>. A 10-mL solution was extracted into the test tube, and 4 mg of maleic acid was added. Subsequently, 0.5 mL of the above solution and 50 µL of D<sub>2</sub>O were injected into a nuclear magnetic tube for NMR detection. As for the calibration curve, a series of <sup>15</sup>NH<sub>4</sub><sup>+-15</sup>N solutions (<sup>15</sup>NH<sub>4</sub><sup>+-15</sup>N concentration and the area ratio in the NMR spectra were positively correlated, the calibration was achieved using the peak area ratio between <sup>15</sup>NH<sub>4</sub><sup>+-15</sup>N and maleic acid. Similarly, the amount of <sup>14</sup>NH<sub>4</sub><sup>+-14</sup>N was quantified using the same method as above, where <sup>14</sup>KNO<sub>3</sub> was used as the feeding N-source.

#### **Computational formula**

For nitrate electro-reduction, the yield rate was calculated by Equation 5:

$$NH_3$$
 yield rate  $\left(mg h^{-1} mg_{cat.}^{-1}\right) = \frac{CNH_3 \times V}{t \times m_{cat.}}$  (Equation 5)

FEs of NH<sub>3</sub> and NO<sub>2</sub> were calculated by Equation 6 and 7:

$$FE_{\rm NH_3}(\%) = \frac{8F \times CNH_3 \times V}{17 \times Q}$$
 (Equation 6)

$$FE_{NO_2}(\%) = \frac{2F \times CNO_2 \times V}{46 \times Q}$$

(Equation 7)

where CNH<sub>3</sub> (mg mL<sup>-1</sup>) and CNO<sub>2</sub> (mg mL<sup>-1</sup>) are the measured concentrations of NH<sub>3</sub> and NO<sub>2</sub><sup>-</sup>, respectively. V (mL) is the volume of the cathodic electrolyte, t (h) is the reduction time, m<sub>cat.</sub> (mg) is the mass loading of the catalyst on CC, F (96485 C mol<sup>-1</sup>) is the Faraday constant, and Q (C) is the total charge passing the electrode.

#### **Theoretical simulation**

#### MD simulations

MD simulations were performed by using the Forcite Dynamic program. The simulation system was constructed by stacking a liquid phase onto the surface of BTC/La- $Co_3O_{4-x}$  and  $Co_3O_4$ . The catalyst of La- $Co_3O_{4-x}$  was not considered because we mainly used the MD simulations to prove the function of organic ligands. A typical unit cell model for cubic  $Co_3O_4$  (8.0850 × 8.0850 × 8.0850) was used and then the (111) crystal plane was cleaved. The final model was a 4  $\times$  4 unit cell of Co<sub>3</sub>O<sub>4</sub> (111) surface with two layers. For BTC/La-Co<sub>3</sub>O<sub>4-x</sub>, an octahedral Co was substituted by the La atom, and an adjacent O atom was deleted to simulate the La-doped  $Co_3O_4$  with oxygen vacancy. One H<sub>3</sub>BTC molecule was bonded with an La atom. The liquid phase of KOH solution and KOH solution with NO3<sup>-</sup> were constructed by an amorphous cell module with COMPASSII force field and force field assigned charge calculation methods at 298.15 K. The liquid phase in a 2.6 nm  $\times$  2.6 nm  $\times$ 2.6 nm contained 10  $\mathrm{K}^{+},$  10  $\mathrm{OH}^{-},$  and 550 water molecules formed to simulate a 1.0 M KOH solution. Another 10  $NO_3$  was added to form a 1.0 M KOH solution with 10 mM NO<sub>3</sub>. The geometry of the liquid/catalyst systems was first optimized by the Forcite module. The electrostatic interaction was calculated using the Ewald summation with an accuracy of  $1.0 \times 10^{-4}$  kcal mol<sup>-1</sup>, and the van der Waals interaction was calculated using the atom-based summation.<sup>74</sup> Then, 100-ps MD runs were carried out under isothermal-isobaric (NPT) ensemble (298.15 K, 1 bar). Temperature and pressure were controlled by the Nose-Hoover thermostat and the Parrinello-Rahman barostat, respectively. Equations of motion were integrated by the leapfrog algorithm with a time step of 1 fs.

#### **DFT calculations**

All the computations were performed on the basis of the DFT using the Vienna ab initio Simulation Package (VASP) code.<sup>75,76</sup> The exchange-correlation function in the Perdew-Burke-Ernzerhof (PBE) form within a generalized gradient approximation (GGA) was used.<sup>77,78</sup> A typical unit cell model for cubic  $Co_3O_4$  (8.0850 × 8.0850 × 8.0850) was used and then cleaved the (111) crystal plane. The final model was a 2 × 2 × 2 unit cell of  $Co_3O_4$  (111) surface. For La- $Co_3O_{4-x}$ , an octahedral Co was substituted by the La atom, and an adjacent O atom was deleted to simulate the La-doped  $Co_3O_4$  with oxygen vacancy. For BTC/La- $Co_3O_{4-x}$ , one H<sub>3</sub>BTC molecule was bonded with the La atom in the La- $Co_3O_{4-x}$  structure. Moreover, a vacuum spacing of ~15 Å was used to prevent spurious interaction between periodic images. During the calculation, the rock-bottom layer of the model is fixed. A cutoff energy of 450 eV for plain-wave basis sets was adopted, and the convergence criterion of the energy was set to be within 1.0 × 10<sup>-5</sup> eV with forces on each atom less than 0.02 eV/Å. A 3 × 3 × 1 Monkhorst-Pack grid of k-points was selected to sample the Brillouin zone integration.

The  $NO_3^-$  reduction reaction on the surfaces of the catalysts was simulated by the following process:<sup>79</sup>

$$* + NO_3^-(aq) \rightarrow *NO_3 + e^-$$

![](_page_21_Picture_12.jpeg)

![](_page_22_Picture_0.jpeg)

 $^{*}NO_{3} + H_{2}O + e^{-} \rightarrow ^{*}NO_{2}OH + OH^{-}$ 

where asterisks (\*) represent the active sites. For each electrochemical step, the Gibbs free-energy changes ( $\Delta G$ ) for the eNO<sub>3</sub>RR procedures were estimated according to Equation 8:<sup>80</sup>

$$\Delta G = \Delta E + \Delta ZPE - T\Delta S + \Delta G_U + \Delta G_{pH} \qquad (Equation 8)$$

where  $\Delta E$  is the difference of energy calculated by DFT between the reactant and product, and  $\Delta ZPE$  is the change of zero-point energies, which could be evaluated by:

$$ZPE = N_a \sum_i \frac{hv_i}{2}$$

where  $N_a$  is the Avogadro number, h is the Planck constant, and  $\nu_i$  represents the frequency. T is room temperature (298.15 K), and  $\Delta S$  is the change of entropy obtained from the following equation:

$$S = R \sum_{i} \left\{ \frac{\left(\frac{hv_{i}}{k_{B}T}\right) \exp\left(-\frac{hv_{i}}{k_{B}T}\right)}{\left[1 - \exp\left(-\frac{hv_{i}}{k_{B}T}\right)\right]} - \ln\left[1 - \exp\left(-\frac{hv_{i}}{k_{B}T}\right)\right] \right\}$$

where R and  $k_{\text{B}}$  are the universal gas constant and the Boltzmann constant, respectively.

 $\Delta G_U$  is the contribution of electrode potential, which can be calculated by  $\Delta G_U = -eU$ , where e is the number of electrons transferred, U is the applied potential measured against the standard hydrogen electrode, and U = 0 V is considered.  $\Delta G_{pH}$  is the free-energy correction of pH, which can be calculated by  $\Delta G_{pH} = -k_BT \times pH \times \ln 10$ , and pH is set to be 0 and 14, respectively.

To calculate the Gibbs free energy of  $NO_3^-(aq)$  adsorption onto the electrode surface, the process could be divided into three steps, as follows:

$$NO_{3}^{-}(aq) + H^{\scriptscriptstyle +} \rightarrow HNO_{3}(aq) \tag{Equation 9}$$

$$HNO_3(aq) \rightarrow HNO_3(g)$$
 (Equation 10)

$$* + HNO_3(g) \rightarrow ^*NO_3 + \frac{1}{2} H_2 \tag{Equation 11}$$

In Equation 9, the Gibbs free energy from  $NO_3^{-}(aq)$  to  $HNO_3(aq)$  formation is 0.317 eV. The Gibbs free energy for the vaporization of  $HNO_3(aq)$  was -0.074 eV. The Gibbs free energy of  $NO_3$  adsorption on the active site (\* $NO_3$ ) could be calculated as follows:

$$\Delta G_{ads}(*NO_3) = G(*NO_3) + \frac{1}{2}G_{gas}(H_2) - G(*) - G_{gas}(HNO_3)$$

Thus, the change of Gibbs free energy of NO<sub>3</sub> adsorption from the solution phase to the electrode surface for, i.e., \* + NO<sub>3</sub><sup>-</sup>(aq)  $\rightarrow$  \*NO<sub>3</sub> + e<sup>-</sup> could be calculated as follows:

$$\Delta G(*NO_3) = \Delta G_{ads}(*NO_3) + 0.074 \text{ eV} + 0.317 \text{ eV} - \Delta G_{correct}$$

 $\Delta G_{\text{correct}}$  is the correction of adsorption energy. The thermodynamic values (0.317 eV and 0.074 eV) are obtained from the CRC Handbook of Chemistry and Physics.<sup>81</sup>

#### SUPPLEMENTAL INFORMATION

Supplemental information can be found online at https://doi.org/10.1016/j.checat. 2024.101024.

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#### **AUTHOR CONTRIBUTIONS**

D.C. and S.Z. contributed equally to this work. D.C., S.Z., D.Y., and Y.Z. carried out the synthesis, electrochemical measurements, and computational calculations. Q.Q., W.W., Y.M., and X.L. conducted part of the characterizations. D.C. and S.Z. participated in the analysis of the data. S.Y., T.Y., C.Z., and J.C.H. directed this work. All authors discussed and revised the manuscript.

#### **DECLARATION OF INTERESTS**

The authors declare no competing interests.

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